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L1	52311	Mo near25 v	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:06
L3	27957	L1 near25 (Te or Sb or Nb)	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:02
L4	4371	I3 Near25 O	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:59
L5	25996	L1 near25 (Te or Nb)	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:09
L6	4030	L5 Near25 O	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:09
L7	42436	("562").CLAS.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	OFF	2005/08/11 06:09
L8	99	16 and 17	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:10
L11	232	562/549.ccls.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:13
L12	25	l8 and l11	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:12
L13	184	562/547.ccls.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:13
L14	28	18 and 113	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:56
L15	6	US-5281745-\$.DID. OR US-5380933-\$. DID. OR US-6043185-\$.DID.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 06:56

L16	2545	L1 near25 (Te)	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:02
L17	1239	L16 near25 (Zn)	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:05
L18	5	I13 and I17	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:03
L19	1105	L16 near25 (Au)	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:17
L20	2	I13 and I19	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:05
L21	1331	L16 near25 (Pb)	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:17
L22	397	l11 or l13	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:17
L23	5	l21 and l22	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON .	2005/08/11 07:52
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L25	1	"5191116".PN.	USPAT; USOCR	OR	ON	2005/08/11 07:22
L26	1	"5210293".PN.	USPAT; USOCR	OR	ON	2005/08/11 07:23
L27	1	"5371306".PN.	USPAT; USOCR	OR	ON	2005/08/11 07:23
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L29	1	"5371306".PN.	USPAT; USOCR	OR	ON	2005/08/11 07:24
L30	1	"5380933".PN.	USPAT; USOCR	OR	ON	2005/08/11 07:24

L31	2	"2001342169"	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2005/08/11 07:53
L32	10	(((acrylic or methacrylic) and l4)and (propane or isobutane or alkene)).clm.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR .	ON	2005/08/11 08:02
L33	7	(((acrylic or methacrylic) and I4)and (propane or isobutane or alkene)).clm.	US-PGPUB	OR	ON	2005/08/11 08:24
L34	0	"6746983".pn.	US-PGPUB	OR	ON	2005/08/11 08:24
L35	2	("6746983").PN.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	OFF	2005/08/11 08:25

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L1 73968 MO(L)V

=> L1(1) (Te or Sb or Nb)

66710 TE

1743 TES

68224 TE

(TE OR TES)

99316 SB

3931 SBS

103078 SB (SB OR SBS) 117860 NB 6944 NBS 124614 NB (NB OR NBS) 23615 L1(L) (TE OR SB OR NB) L2=> acrylic or methacrylic 249008 ACRYLIC 1304 ACRYLICS 249378 ACRYLIC (ACRYLIC OR ACRYLICS) 71423 METHACRYLIC 6 METHACRYLICS 71427 METHACRYLIC (METHACRYLIC OR METHACRYLICS) L3 285147 ACRYLIC OR METHACRYLIC => 12 and 13 305 L2 AND L3 => propane 76732 PROPANE 1110 PROPANES L5 77305 PROPANE (PROPANE OR PROPANES) => 14 and 15 118 L4 AND L5 => d 16 108-118 ti ANSWER 108 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN 1.6 Method and catalysts for producing acrylic acid from ΤI propane and gaseous oxygen ANSWER 109 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN 1.6 ΤI Process for simultaneous preparation of acrylonitrile and acrylic ANSWER 110 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN 1.6 Preparation of catalysts for acrylic acid preparation ΤI 1.6 ANSWER 111 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN Preparation of acrylic acid from propane using mixed ΤI metal oxide catalysts ANSWER 112 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN L6 Preparation of metal oxide catalysts for oxidation of propane at TΙ gas phase ANSWER 113 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN L6 Preparation of mixed metal oxide catalysts and preparation of ΤI acrylic acid from propane by using the catalysts ANSWER 114 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN L6 One-step preparation of (meth)acrylic acid by catalytic ΤI oxidation of propane or isobutane ANSWER 115 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN L6 Novel Catalysts for the Environmentally Friendly Synthesis of Methyl TI Methacrylate

ANSWER 116 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN

L6

Unsaturated carboxylic acid by oxidation of alkane using certain mixed metal oxides.

L6 ANSWER 117 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN Acroleins from propylenes

Catalysts for oxidation of propylene to acrolein or acrylic acid

- => d 16 113-114, 118 ti fbib abs
- L6 ANSWER 113 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Preparation of mixed metal oxide catalysts and preparation of acrylic acid from propane by using the catalysts

ANSWER 118 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN

- AN 1998:143244 CAPLUS
- DN 128:192371

L6

ΤI

- TI Preparation of mixed metal oxide catalysts and preparation of acrylic acid from propane by using the catalysts
- IN Ushikubo, Takashi; Kinoshita, Hisao; Watanabe, Akira
- PA Mitsubishi Chemical Industries Ltd., Japan
- SO Jpn. Kokai Tokkyo Koho, 6 pp. CODEN: JKXXAF
- DT Patent
- LA Japanese
- FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
ΡI	JP 10057813	A2	19980303	JP 1996-221139	19960822
				JP 1996-221139	19960822

- AB The title catalysts are prepared by drying solns. or slurries containing Mo, V, and Te and/or Sb, heating under substantially O-free atmospheric, then heating under O-containing gas. Acrylic acid is prepared by gas-phase oxidation of propane by using the catalysts. A gaseous mixture of propane, air, and steam was introduced to a fixed bed reactor filled with a catalyst prepared by heating MolVO.3TeO.23NbO.12On, then treated at 380° for 2 h to give 52.5% acrylic acid.
- L6 ANSWER 114 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN
- TI One-step preparation of (meth)acrylic acid by catalytic oxidation of propane or isobutane
- AN 1997:784172 CAPLUS
- DN 128:48601
- TI One-step preparation of (meth)acrylic acid by catalytic oxidation of propane or isobutane
- IN To, Shinrin; Takahashi, Mamoru; Ishii, Masakazu
- PA Toa Gosei Chemical Industry Co., Ltd., Japan
- SO Jpn. Kokai Tokkyo Koho, 4 pp. CODEN: JKXXAF
- CODEN: JK
- DT Patent
- LA Japanese
- FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
ΡI	JP 09316023	A2	19971209	JP 1996-153465	19960524
				JP 1996-153465	19960524

AB Propane or isobutane is catalytically oxidized in gas phase in the presence of catalysts containing Mo, Sb, V,
O, and A (A represents ≥1 elements selected from Nb, Ta,
Sn, W, Ti, Ni, Fe, Cr, and Co) to give (meta)acrylic acids.
Oxidation of propane with O2 at 400° for 10 h in the presence of a catalyst prepared from ammonium metavanadate, antimony oxide, ammonium molybdate, and niobic acid gave acrylic acid (I) in high yield with conversion 30.9% and I selectivity 29.5%.

1.6 ANSWER 118 OF 118 CAPLUS COPYRIGHT 2005 ACS on STN ΤI Catalysts for oxidation of propylene to acrolein or acrylic acid AN 1969:449291 CAPLUS DN 71:49291 Catalysts for oxidation of propylene to acrolein or acrylic acid TI Kashiwabara, Hideyuki; Nakamura, Yasushi IN PΑ Asahi Electro-Chemical Co., Ltd. so Jpn. Tokkyo Koho, 8 pp. CODEN: JAXXAD DT Patent LA Japanese FAN.CNT 1 PATENT NO. KIND DATE APPLICATION NO. \_\_\_\_\_ --------------PΙ JP 43024645 B4 19681024 JΡ 19660418 In manufacturing acrolein (I) or acrylic acid (II) or a mixture of I and II by catalytic reaction in gaseous propylene (III) and O, catalytic systems containing Mo, V, W, Te, Sb, Sn, or Bi, with O, were used. In an example, a solution of 72.0 parts MoO3 and 40.2 parts H2WO4.H2O in NH4OH, an aqueous solution of 11.7 parts NH4VO3, a solution of 70.1 parts SnCl4.5H2O in aqueous HCl and a solution of 3.2 parts Te in HNO3 were mixed and gradually evaporated to dryness with stirring vigorously on the water bath. The catalyst (between 6-20 mesh in a quartz tube) was heated in air stream at .apprx.470° 4 hrs. and at 358-470° for .apprx.2 hrs., then in O stream at 150-358° 3 hrs. to yield a catalytic mixture (IV): atomic ratio given, Mo-V-W-Te-Sn 5:1:1.5:0.5:2. A mixture of crude III (93% III, main impurities: propane, ethane), O and steam (mole ratio, III-O-H2O 1:1.6:6) was introduced into a stainless-steel tube filled with IV at 450° under the atmospheric pressure at apparent contact time of 3 sec. to yield II containing I, AcOH, and AcH yielded II; % conversion III-II = 66.5%. => Nb 117860 NB 6944 NBS L7 124614 NB (NB OR NBS) => 16 not 17 28 L6 NOT L7 L8=> d 18 18-28 ti ANSWER 18 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN 1.8 Production method of (meth) acrylic acid using mixed metal TIoxidation catalysts ANSWER 19 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN L8TI Method for producing acrylic acid by the heterogeneously catalyzed gas-phase oxidation of propane L8 ANSWER 20 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN TI Manufacture of metal oxide catalyst containing Mo, V, and Sb ANSWER 21 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN L8TI Manufacture of acrylonitrile and/or'of acrylic acid with mixed metal oxide catalysts from propane with low sulfur content ANSWER 22 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN L8 Catalytic performance of hydrothermally synthesized Mo-V

-M-O (M = Sb or Te) oxides in the selective oxidation

ΤI

## of light paraffins

- L8 ANSWER 23 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Catalytic oxidative activation of light alkanes over Mo-V-based oxides having controlled surface
- L8 ANSWER 24 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Selective oxidation of light alkanes over hydrothermally synthesized Mo-V-M-O (M = Al, Ga, Bi, Sb, and Te ) oxide catalysts
- L8 ANSWER 25 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Process for simultaneous preparation of acrylonitrile and acrylic acid
- L8 ANSWER 26 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Preparation of mixed metal oxide catalysts and preparation of acrylic acid from propane by using the catalysts
- L8 ANSWER 27 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Acroleins from propylenes
- L8 ANSWER 28 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Catalysts for oxidation of propylene to acrolein or acrylic acid
- => d 18 18-24,26,28 ti fbib abs
- L8 ANSWER 18 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Production method of (meth)acrylic acid using mixed metal oxidation catalysts
- AN 2002:235898 CAPLUS
- DN 136:263583
- TI Production method of (meth)acrylic acid using mixed metal oxidation catalysts
- IN Ueda, Wataru
- PA Mitsubishi Rayon Co., Ltd., Japan
- SO Jpn. Kokai Tokkyo Koho, 5 pp. CODEN: JKXXAF
- DT Patent
- LA Japanese
- FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
ΡI	JP 2002088012	A2	20020327	JP 2000-276096	20000912
				JP 2000-276096	20000912

- Disclosed is production methods of (meth)acrylic acid by oxidizing propane or isobutane in gas-phase in the presence of an oxidation catalyst having general formula MoaVbTecFedMeOx, wherein Mo = molybdenum, V = vanadium, Te = tellurium, Fe = iron, M = at least one element selected from chromium, manganese, cobalt, nickel, aluminum, titanium, tin, bismuth, cerium, and tungsten, O = oxygen, a,b,c,d,e,x = atomic ratio.
- L8 ANSWER 19 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Method for producing acrylic acid by the heterogeneously catalyzed gas-phase oxidation of propane
- AN 2002:72014 CAPLUS
- DN 136:118851
- TI Method for producing acrylic acid by the heterogeneously catalyzed gas-phase oxidation of propane
- IN Borgmeier, Frieder; Tenten, Andreas; Hibst, Hartmut; Mueller-Engel, Klaus Joachim; Unverricht, Signe; Cox, Gerhard
- PA Basf Aktiengesellschaft, Germany
- SO PCT Int. Appl., 34 pp.

CODEN: PIXXD2

DТ Patent German LA FAN.CNT 5 PATENT NO. DATE KIND APPLICATION NO. DATE -----------**---**----------PΙ WO 2002006199 20020124 WO 2001-EP8178 A2 20010716 WO 2002006199 **A**3 20020523 AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW, AM, AZ, BY, KG, KZ, MD, RU, TJ, TM RW: GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW, AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR, BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG DE 2000-10034825 A 20000718 DE 2000-10046672 A 20000920 DE 2001-10118814 A 20010417 DE 2001-10119933 A 20010423 20020131 DE 10034825 A1 DE 2000-10034825 20000718 DE 10046672 A1 20020328 DE 2000-10046672 20000920 DE 10118814 A1 20021024 DE 2001-10118814 20010417 DE 10119933 A1 20021024 DE 2001-10119933 20010423 EP 1301457 A2 20030416 EP 2001-967180 20010716 R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT, IE, SI, LT, LV, FI, RO, MK, CY, AL, TR DE 2000-10034825 A 20000718 DE 2000-10046672 A 20000920 DE 2001-10118814 A 20010417 DE 2001-10119933 A 20010423 W 20010716 WO 2001-EP8178 BR 2001012557 BR 2001-12557 Α 20030722 20010716 DE 2000-10034825 A 20000718 DE 2000-10046672 A 20000920 DE 2001-10118814 A 20010417 A 20010423 DE 2001-10119933 W 20010716 WO 2001-EP8178 JP 2004504288 T2 JP 2002-512106 20040212 20010716 DE 2000-10034825 A 20000718 DE 2000-10046672 A 20000920 Α DE 2001-10118814 20010417 DE 2001-10119933 Α 20010423 W WO 2001-EP8178 20010716 US 2003187298 **A1** 20031002 US 2003-333060 20030116 US 6867328 B2 20050315 DE 2000-10034825 A 20000718 Α DE 2000-10046672 20000920 Α DE 2001-10118814 20010417 DE 2001-10119933 · A 20010423 W WO 2001-EP8178 20010716 US 2004102648 **A**1 20040527 US 2003-399039 20030417 WO 2001-EP11909 W 20011016 PATENT FAMILY INFORMATION: FAN 2001:923733 PATENT NO. KIND DATE APPLICATION NO. DATE -----\_\_\_\_ ----------------WO 2001096270 A2 20011220 WO 2001-EP6528 20010608 PΙ W: AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT,

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   R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT,
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       GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PH, PL,
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		BF,	BJ,	CF,	CG,	CI,	CM,	GA,			, GW, 2001-						
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                                           DE 2001-10118814
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                                           WO 2002-EP4073
                                                              W 20020412
     A method for producing acrylic acid by the heterogeneously
     catalyzed gas-phase oxidation of propane on a multi-metal oxide
     mass, which contains the elements Mo, V, Te,
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AB and/or Sb, and optionally others, and has a specific X-ray diffractogram; X-ray diffractogram are presented.

- ANSWER 20 OF 28 CAPLUS COPYRIGHT, 2005 ACS on STN L8
- Manufacture of metal oxide catalyst containing Mo, V, TI and Sb
- AN 2001:910040 CAPLUS
- 136:43534 DN
- Manufacture of metal oxide catalyst containing Mo, V, ΤI
- Takahashi, Mamoru; Tu, Xin Lin; Adzuma, Hiroshi IN
- Toa Gosei Chemical Industry Co., Ltd., Japan PA
- Jpn. Kokai Tokkyo Koho, 5 pp. SO CODEN: JKXXAF
- DT Patent
- LA Japanese
- FAN.CNT 1

	PATENT NO.	KIND DATE		APPLICATION NO.	DATE	
ΡI	JP 2001347165	A2	20011218	JP 2000-172857	20000609	
				JP 2000-172857	20000609	

- The invention relates to a manufacture of metal oxide catalyst which is used AB for the production of acrylic acid from propane at high The process comprises effecting a reaction of an Sb(III) -containing compound with an oxidizing agent to oxidize Sb(III) to Sb(V), and adding a V(V)-containing compound and heating to  $\leq 70^{\circ}$  to convert the remaining Sb(III) to Sb(V).
- ANSWER 21 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN L8
- Manufacture of acrylonitrile and/or of acrylic acid with mixed TI metal oxide catalysts from propane with low sulfur content
- 2001:892150 CAPLUS ΑN
- DN 136:38021
- Manufacture of acrylonitrile and/or of acrylic acid with mixed ΤI metal oxide catalysts from propane with low sulfur content
- Ushikubo, Takashi IN
- Mitsubishi Chemical Corp., Japan PA

SO Jpn. Kokai Tokkyo Koho, 5 pp.

CODEN: JKXXAF

DT Patent

LA Japanese FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
ΡI	JP 2001342169	A2	20011211	JP 2000-167076	20000605
				JP 2000-167076	20000605

AB H2C:CHCN and/or H2C:CHCO2H are manufactured by gas-phase oxidation of propane in the presence of mixed metal oxide catalysts containing Mo, V, Te, and/or Sb with

controlling S content of gas supplied to a reactor to  $\leq 200$  ppm. Thus, a gaseous mixture (containing 0.235 ppm S) of **propane**, NH3, O, and N was passed through a fixed bed reactor in the presence of Mo1V0.3Te0.16Nb0.12On/SiO2 over 300 h to show almost no catalyst deactivation.

- L8 ANSWER 22 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Catalytic performance of hydrothermally synthesized Mo-V
  -M-O (M = Sb or Te) oxides in the selective oxidation
  of light paraffins
- AN 2001:608688 CAPLUS
- DN 136:151474
- TI Catalytic performance of hydrothermally synthesized Mo-V
  -M-O (M = Sb or Te) oxides in the selective oxidation of light paraffins
- AU Oshihara, Kenzo; Hisano, Tokio; Kayashima, Youhei; Ueda, Wataru
- CS Department of Materials Science and Engineering, Science University of Tokyo in Yamaguchi, Yamaguchi, 756-0884, Japan
- SO Studies in Surface Science and Catalysis (2001), 136(Natural Gas Conversion VI), 93-98
  CODEN: SSCTDM; ISSN: 0167-2991
- PB Elsevier Science B.V.
- DT Journal
- LA English
- AB Hydrothermally synthesized Mo6V2Sb10x and Mo6V3Te10x mixed oxide catalysts were evaluated for methane, ethane and propane oxidation. The catalysts were very active for oxidative dehydrogenation of ethane with 80% ethylene selectivity, nearly independently of reaction temperature (300-400°). Grinding-treatment made the catalyst more selective by suppressing COx production. The catalysts were inactive for methane oxidation, but they were highly active for propane oxidation to acrylic acid.
- RE.CNT 8 THERE ARE 8 CITED REFERENCES AVAILABLE FOR THIS RECORD ALL CITATIONS AVAILABLE IN THE RE FORMAT
- L8 ANSWER 23 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN
- TI Catalytic oxidative activation of light alkanes over Mo-V-based oxides having controlled surface
- AN 2001:549480 CAPLUS
- DN 135:318188
- TI Catalytic oxidative activation of light alkanes over Mo-V-based oxides having controlled surface
- AU Oshihara, Kenzo; Hisano, Tokio; Ueda, Wataru
- CS Department of Materials Science and Engineering, Science University of Tokyo in Yamaguchi, Yamaguchi, 765-0884, Japan
- SO Topics in Catalysis (2001), 15(2-4), 153-160 CODEN: TOCAFI; ISSN: 1022-5528
- PB Kluwer Academic/Plenum Publishers
- DT Journal
- LA English
- OS CASREACT 135:318188
- AB An arrangement of catalytically active elements of Mo, V , and Te in an oxide solid with a single crystallog. phase was

successfully done by the hydrothermal synthetic method. A black solid powder with a rod-shape (by SEM) was obtained. This catalyst material was first air-treated at 280° for 2 h, by which Te was stabilized in the structure. The air-treated sample was then heat-treated at 600° in a N stream. It was revealed by XRD anal. that this treatment made the solid in a well-crystallized state. Finally, to break the rods into fine powders, the well-crystallized rod-shaped material was ground, by which a face of the cross-section of the rods seems to be preferentially appeared. Thus obtained catalyst, Mo6V3Te10x, showed a high activity for the selective oxidation of propane to acrylic acid at 360°. Since the grinding is the most effectual determinant in the propane conversion and the acrylic acid formation, the surface on the cross-section part of the rod-shaped crystals is active for the selective oxidation It was assumed that all the elements of Mo, V, and Te arrange in this surface and effectively promote the consecutive oxidation from propane to acrylic acid via propene and acrolein. THERE ARE 17 CITED REFERENCES AVAILABLE FOR THIS RECORD ALL CITATIONS AVAILABLE IN THE RE FORMAT ANSWER 24 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN Selective oxidation of light alkanes over hydrothermally synthesized Mo-V-M-O (M = Al, Ga, Bi, Sb, and Te ) oxide catalysts 2000:564783 CAPLUS 133:335477 Selective oxidation of light alkanes over hydrothermally synthesized Mo-V-M-O (M = Al, Ga, Bi, Sb, and Te ) oxide catalysts Ueda, W.; Oshihara, K. Department of Materials Science and Engineering, Science University of Tokyo in Yamaguchi, Yamaguchi, 765-0884, Japan Applied Catalysis, A: General (2000), 200(1-2), 135-143 CODEN: ACAGE4; ISSN: 0926-860X Elsevier Science B.V. Journal English Selective oxidns. of ethane to ethene and acetic acid and of propane to acrylic acid were carried out over hydrothermally synthesized Mo-V-M-O (M = Al, Ga, Bi, Sb, and Te) complex metal oxide catalysts. All the synthesized solids were rod-shaped crystallites and gave a common XRD peak corresponding to 4.0 A d-spacing. From the different XRD patterns at low angle region below 10° and from the different shape of the cross-section of the rod crystal obtained by SEM, the solids were

hydrothermally synthesized Mo-V-M-O (M = Al, Ga, Bi, Sb, and Te) complex metal oxide catalysts. All the synthesized solids were rod-shaped crystallites and gave a common XRD peak corresponding to 4.0 A d-spacing. From the different XRD patterns at low angle region below 10° and from the different shape of the cross-section of the rod crystal obtained by SEM, the solids were classified into two groups: Mo-V-M-O (M = Al, possibly Ga and Bi) and Mo-V-M-O (M=Sb, and Te). The former catalyst was moderately active for the ethane oxidation to ethene and to acetic acid. On the other hand the latter was found to be extremely active for the oxidative dehydrogenation. The Mo-V-M-O (M = Sb, and Te) catalysts were also active for the propane oxidation to acrylic acid. It was found that the grinding of the catalysts after heat-treatment at 600°C in N2 increased the conversions of propane and enhanced the selectivity to acrylic acid. Structural arrangement of the catalytic functional components on the surface of the cross-section of the rod-shaped catalysts seems to be important for the oxidation activity and selectivity.

RE.CNT 29 THERE ARE 29 CITED REFERENCES AVAILABLE FOR THIS RECORD

L8 ANSWER 26 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN

TI Preparation of mixed metal oxide catalysts and preparation of acrylic acid from propane by using the catalysts

ALL CITATIONS AVAILABLE IN THE RE FORMAT

AN 1998:143244 CAPLUS

T.R

TΙ

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DN 128:192371

TI Preparation of mixed metal oxide catalysts and preparation of acrylic acid from propane by using the catalysts

IN Ushikubo, Takashi; Kinoshita, Hisao; Watanabe, Akira

PA Mitsubishi Chemical Industries Ltd., Japan

SO Jpn. Kokai Tokkyo Koho, 6 pp.

CODEN: JKXXAF

DT Patent

LA Japanese

FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE		
ΡI	JP 10057813	A2	19980303	JP 1996-221139	19960822		
				JP 1996-221139	19960822		

AB The title catalysts are prepared by drying solns. or slurries containing Mo, V, and Te and/or Sb, heating under substantially O-free atmospheric, then heating under O-containing gas. Acrylic acid is prepared by gas-phase oxidation of propane by using the catalysts. A gaseous mixture of propane, air, and steam was introduced to a fixed bed reactor filled with a catalyst prepared by heating Mo1V0.3Te0.23Nb0.12On, then treated at 380° for 2 h to give 52.5% acrylic acid.

L8 ANSWER 28 OF 28 CAPLUS COPYRIGHT 2005 ACS on STN

TI Catalysts for oxidation of propylene to acrolein or acrylic acid

AN 1969:449291 CAPLUS

DN 71:49291

TI Catalysts for oxidation of propylene to acrolein or acrylic acid

KIND DATE

IN Kashiwabara, Hideyuki; Nakamura, Yasushi

PA Asahi Electro-Chemical Co., Ltd.

SO Jpn. Tokkyo Koho, 8 pp.

CODEN: JAXXAD

DT Patent

LA Japanese

PATENT NO.

66.5%.

FAN.CNT 1

	-			
	TD 42004645	D4 10601024	TD	10000419
ΡI	JP 43024645			19660418
AB				or a mixture of I and
	II by catalytic react	ion in gaseous	propylene (II)	<ul><li>I) and O, catalytic</li></ul>
	systems containing Mc	o, V, W, Te, Sb,		
				olution of 72.0 parts MoO3
				ition of 11.7 parts NH4VO3, a
				and a solution of 3.2 parts
	Te in HNO3 were mixed			
				yst (between 6-20 mesh in
	a quartz tube) was he			
	at 358-470° for .appr			
	3 hrs. to yield a cat			
	V-W-Te-Sn 5:1:1.5:0.5			
	main impurities: prop	oane, ethane), O	and steam (mo	ole ratio,
				s-steel tube filled with
	IV at 450° under the	atmospheric pre	ssure at appai	cent contact time of 3
	sec. to yield II cont	aining I, AcOH,	and AcH yield	ded II; % conversion III-II =

APPLICATION NO.

DATE

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ENTRY SESSION
FULL ESTIMATED COST
BISCOUNT AMOUNTS (FOR QUALIFYING ACCOUNTS)
SINCE FILE TOTAL
ENTRY SESSION
ENTRY SESSION

CA SUBSCRIBER PRICE -8.76 -8.76

SESSION WILL BE HELD FOR 60 MINUTES
STN INTERNATIONAL SESSION SUSPENDED AT 07:53:46 ON 11 AUG 2005